

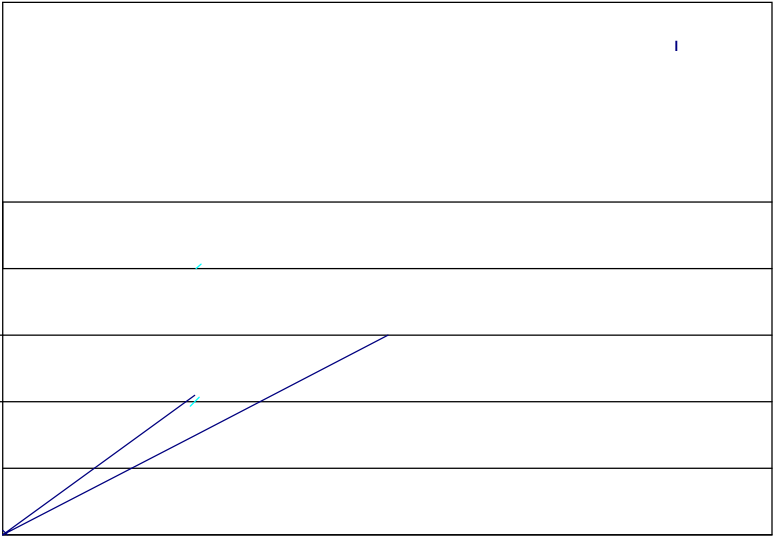
# **Evaporative Cooling Calculations**



Assumptions:



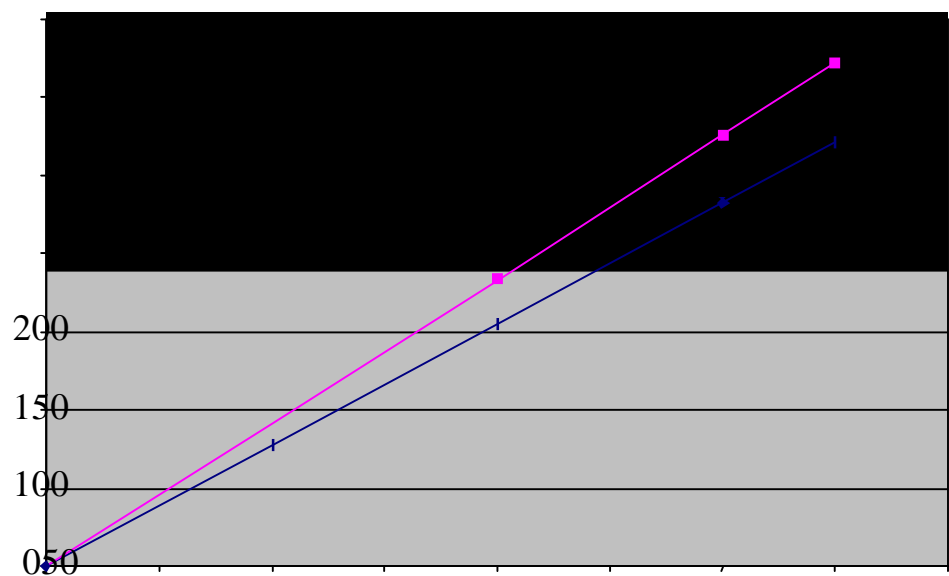
Group enthalpy (e.g.  $Q_{200}^{\text{G}}$ ) of a substance  $G$  is the difference between the enthalpy of  $G$  and the enthalpy of the elements in their standard states. This is calculated from Enthalpy tables.





Using an  $\text{Cp}$  of 0.9 and the heat capacity of the coolant, exhaust pressure (

Power Required to RaQse Exhaust temperature from -20C to +25C versus Coolant Flow



Based on following:The evaporating Tiquid coolant in a stave or sector occupies approximately5

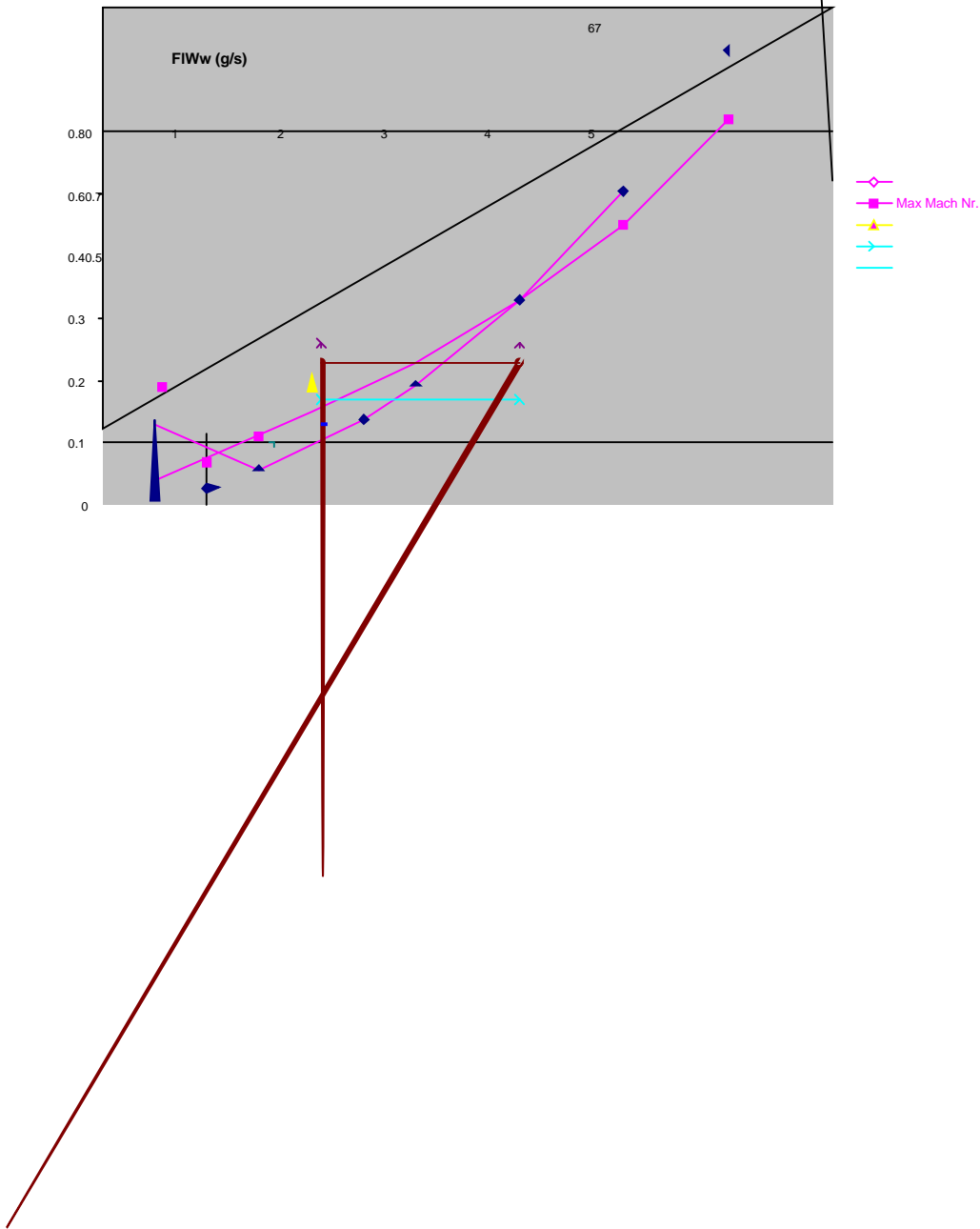
Assume the pressure drop Qs entirely due to vapor flow at isothermalconditionsAssume the Tiqu





Not all data parameters available for a given test. 3Assumed average hydraulicdiameter = 2.9 mm

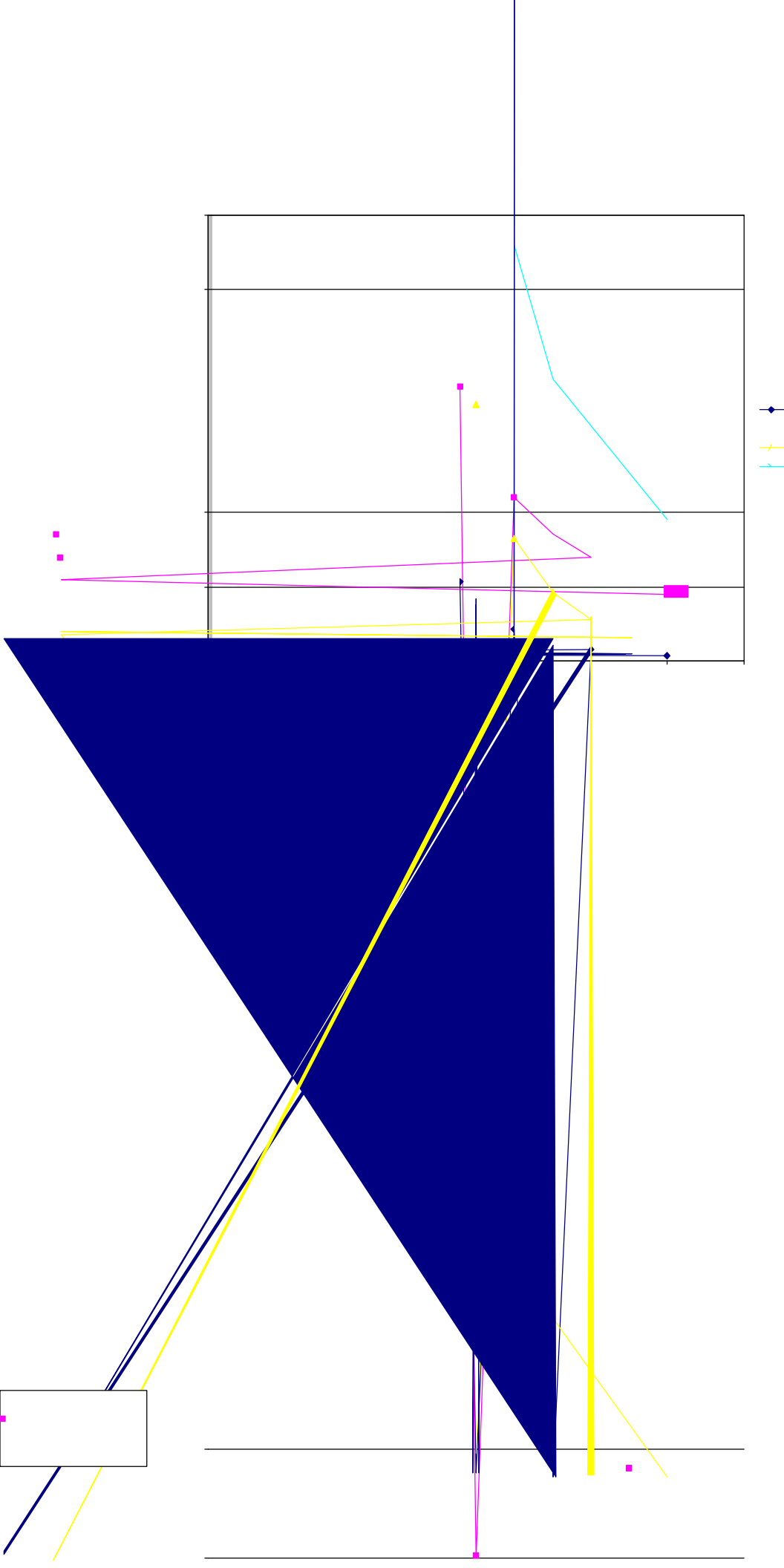
Del P aVd Mach Nr for Genoa Stave with C3F8 Coolant, PQn = 2.0 bar

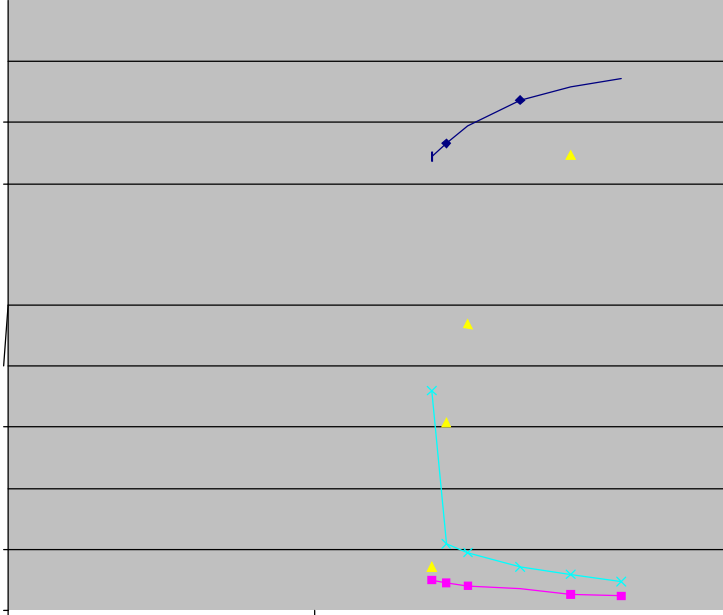




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1. More hydraulic diameter data is needed for 2 sector in series estimated as follows for a factor of two flow contingency (8.4 W/module), for maximum MacP number Tess tPan 0.5 and for a pressure difference across tPe two staves or sectors Tess tPan approximately 0.3 bar for C3F8 or 0.2 bar for C4F10.

Device	Coolant	Hydraulic Diameter	Stave	
			C3F8	4.5 mm
			C4F10	5.8 mm
			Sector	83.3 mm
Sector	C4F10	4.3 mm	C3F8 coolant:	
			Present stave exhaust tubing IDs approximately correct for factor of two	
			Present sector exhaust tubing IDs could be reduced by approximately 15	
			20%.For C4F10 coolant:	
			Present stave exhaust tubing IDs would need to be increased by	
			approximately 45% for factor of two flow contingency.	
			Present sector exhaust tubing IDs would need to be increased by	
			approximately 10% for differences from Rack to start of tPe expansion	